

# CHALMERS

## UNIVERSITY OF TECHNOLOGY

### SSY281 - MODEL PREDICTIVE CONTROL

NIKOLCE MURGOVSKI

Division of Systems and Control  
Department of Electrical Engineering  
Chalmers University of Technology  
Gothenburg, Sweden

2021-01-19

# Lecture 1: Introduction and course overview

Goals for today:

- To know about the background of MPC and the ideas behind the course
- To get motivated by being reminded about the limitations of linear design
- To understand the receding horizon control (RHC) idea
- To understand how the course is organized
- To understand the learning objectives of the course

# Background on MPC

- The origin:

# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).

# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).
  - Dynamic Matrix Control (DMC).

# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).
  - Dynamic Matrix Control (DMC).
- Early drivers:

# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).
  - Dynamic Matrix Control (DMC).
- Early drivers:
  - Operation close to limits  $\Rightarrow$  linear control shortcomings.

# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).
  - Dynamic Matrix Control (DMC).
- Early drivers:
  - Operation close to limits  $\Rightarrow$  linear control shortcomings.
  - Large returns on small improvements in e.g. product quality or energy/material consumption.



# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).
  - Dynamic Matrix Control (DMC).
- Early drivers:
  - Operation close to limits  $\Rightarrow$  linear control shortcomings.
  - Large returns on small improvements in e.g. product quality or energy/material consumption.
  - Slow time scale allows time-consuming computations.

# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).
  - Dynamic Matrix Control (DMC).
- Early drivers:
  - Operation close to limits  $\Rightarrow$  linear control shortcomings.
  - Large returns on small improvements in e.g. product quality or energy/material consumption.
  - Slow time scale allows time-consuming computations.
- Limitations of linear control design:

# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).
  - Dynamic Matrix Control (DMC).
- Early drivers:
  - Operation close to limits  $\Rightarrow$  linear control shortcomings.
  - Large returns on small improvements in e.g. product quality or energy/material consumption.
  - Slow time scale allows time-consuming computations.
- Limitations of linear control design:
  - Saturation on control and control rates.

# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).
  - Dynamic Matrix Control (DMC).
- Early drivers:
  - Operation close to limits  $\Rightarrow$  linear control shortcomings.
  - Large returns on small improvements in e.g. product quality or energy/material consumption.
  - Slow time scale allows time-consuming computations.
- Limitations of linear control design:
  - Saturation on control and control rates.
  - Process output limitations.

# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).
  - Dynamic Matrix Control (DMC).
- Early drivers:
  - Operation close to limits  $\Rightarrow$  linear control shortcomings.
  - Large returns on small improvements in e.g. product quality or energy/material consumption.
  - Slow time scale allows time-consuming computations.
- Limitations of linear control design:
  - Saturation on control and control rates.
  - Process output limitations.
  - Buffer control (zone objectives).

# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).
  - Dynamic Matrix Control (DMC).
- Early drivers:
  - Operation close to limits  $\Rightarrow$  linear control shortcomings.
  - Large returns on small improvements in e.g. product quality or energy/material consumption.
  - Slow time scale allows time-consuming computations.
- Limitations of linear control design:
  - Saturation on control and control rates.
  - Process output limitations.
  - Buffer control (zone objectives).
- Important attributes of MPC:

# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).
  - Dynamic Matrix Control (DMC).
- Early drivers:
  - Operation close to limits  $\Rightarrow$  linear control shortcomings.
  - Large returns on small improvements in e.g. product quality or energy/material consumption.
  - Slow time scale allows time-consuming computations.
- Limitations of linear control design:
  - Saturation on control and control rates.
  - Process output limitations.
  - Buffer control (zone objectives).
- Important attributes of MPC:
  - MPC handles actuator limitations and process constraints.

# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).
  - Dynamic Matrix Control (DMC).
- Early drivers:
  - Operation close to limits  $\Rightarrow$  linear control shortcomings.
  - Large returns on small improvements in e.g. product quality or energy/material consumption.
  - Slow time scale allows time-consuming computations.
- Limitations of linear control design:
  - Saturation on control and control rates.
  - Process output limitations.
  - Buffer control (zone objectives).
- Important attributes of MPC:
  - MPC handles actuator limitations and process constraints.
  - MPC handles multivariable systems.



# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).
  - Dynamic Matrix Control (DMC).
- Early drivers:
  - Operation close to limits  $\Rightarrow$  linear control shortcomings.
  - Large returns on small improvements in e.g. product quality or energy/material consumption.
  - Slow time scale allows time-consuming computations.
- Limitations of linear control design:
  - Saturation on control and control rates.
  - Process output limitations.
  - Buffer control (zone objectives).
- Important attributes of MPC:
  - MPC handles actuator limitations and process constraints.
  - MPC handles multivariable systems.
  - MPC is model based (step responses, state-space models etc.).

# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).
  - Dynamic Matrix Control (DMC).
- Early drivers:
  - Operation close to limits  $\Rightarrow$  linear control shortcomings.
  - Large returns on small improvements in e.g. product quality or energy/material consumption.
  - Slow time scale allows time-consuming computations.
- Limitations of linear control design:
  - Saturation on control and control rates.
  - Process output limitations.
  - Buffer control (zone objectives).
- Important attributes of MPC:
  - MPC handles actuator limitations and process constraints.
  - MPC handles multivariable systems.
  - MPC is model based (step responses, state-space models etc.).
- Current driving factors:

# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).
  - Dynamic Matrix Control (DMC).
- Early drivers:
  - Operation close to limits  $\Rightarrow$  linear control shortcomings.
  - Large returns on small improvements in e.g. product quality or energy/material consumption.
  - Slow time scale allows time-consuming computations.
- Limitations of linear control design:
  - Saturation on control and control rates.
  - Process output limitations.
  - Buffer control (zone objectives).
- Important attributes of MPC:
  - MPC handles actuator limitations and process constraints.
  - MPC handles multivariable systems.
  - MPC is model based (step responses, state-space models etc.).
- Current driving factors:
  - Development of theory and new application areas.

# Background on MPC

- The origin:
  - Process control in petrochemical industry (1970s).
  - Dynamic Matrix Control (DMC).
- Early drivers:
  - Operation close to limits  $\Rightarrow$  linear control shortcomings.
  - Large returns on small improvements in e.g. product quality or energy/material consumption.
  - Slow time scale allows time-consuming computations.
- Limitations of linear control design:
  - Saturation on control and control rates.
  - Process output limitations.
  - Buffer control (zone objectives).
- Important attributes of MPC:
  - MPC handles actuator limitations and process constraints.
  - MPC handles multivariable systems.
  - MPC is model based (step responses, state-space models etc.).
- Current driving factors:
  - Development of theory and new application areas.
  - Improvements in numerical computations.

## Example: feedback control of a double integrator system

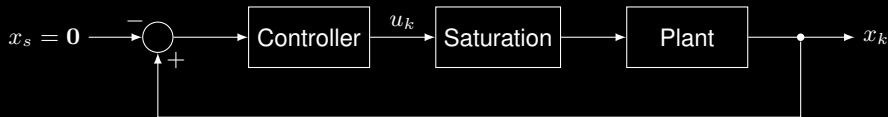
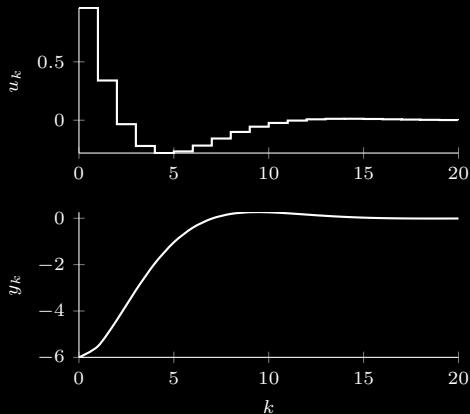


Figure 1: Feedback control loop with input saturation.

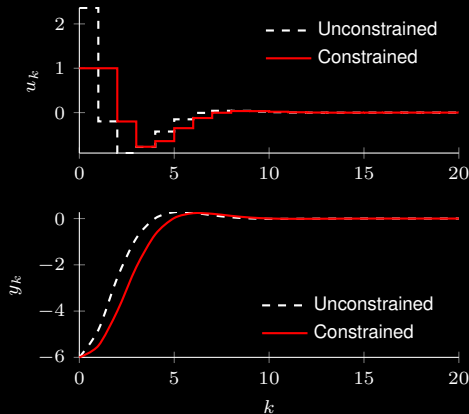
The control input is to be kept within bounds  $u_k \in [-1, 1], \forall k$ . For safety reasons, a saturation function is imposed

$$\text{sat}(u) \triangleq \begin{cases} 1, & u > 1 \\ u, & |u| \leq 1 \\ -1, & u < -1. \end{cases}$$

# LQ control of the double integrator system



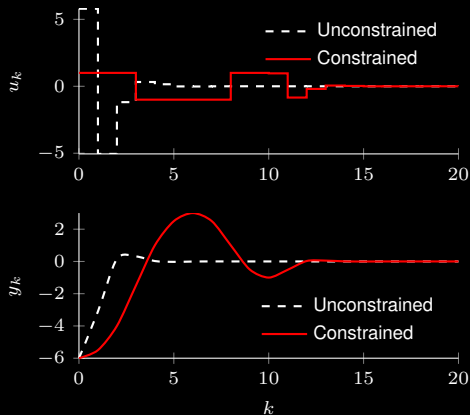
(a) Cautious design with  $u_k = -Kx_k$  and  $R = 20$ .



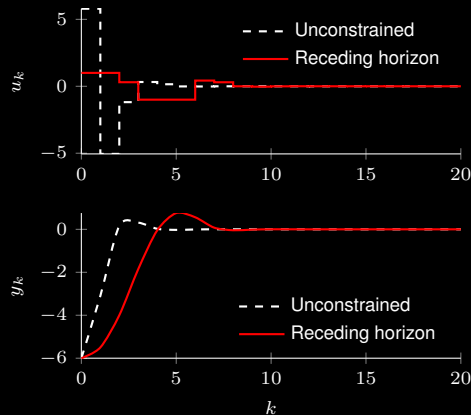
(b) Serendipitous design for constrained and unconstrained LQR with  $u_k = -Kx_k$  and  $u_k = -\text{sat}(Kx_k)$ , respectively, and  $R = 2$ .

Figure 2: LQ control of the double integrator system.

# LQ vs. receding horizon control



(a) Serendipitous design for constrained and unconstrained LQR with  $u_k = -Kx_k$  and  $u_k = -\text{sat}(Kx_k)$ , respectively, and  $R = 0.1$ .



(b) Unconstrained LQR with  $u_k = -Kx_k$  and receding horizon control with  $R = 0.1$ .

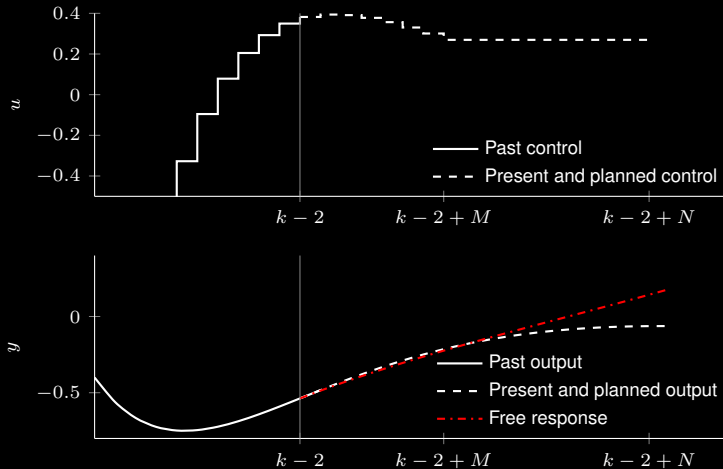
Figure 3: Comparison between LQ and receding horizon control of the double integrator system.

## The receding horizon idea

- a) At time instant  $k$ , *predict* the process response over a finite **prediction horizon**  $N$ ; this response depends on the sequence of future control inputs over the **control horizon**  $M$ .
- b) Pick the control sequence which gives the best performance in terms of a specified **objective**, **cost function** or **criterion**.
- c) Apply the first element in the control sequence to the process, discard the rest of the sequence, and return to step 1.

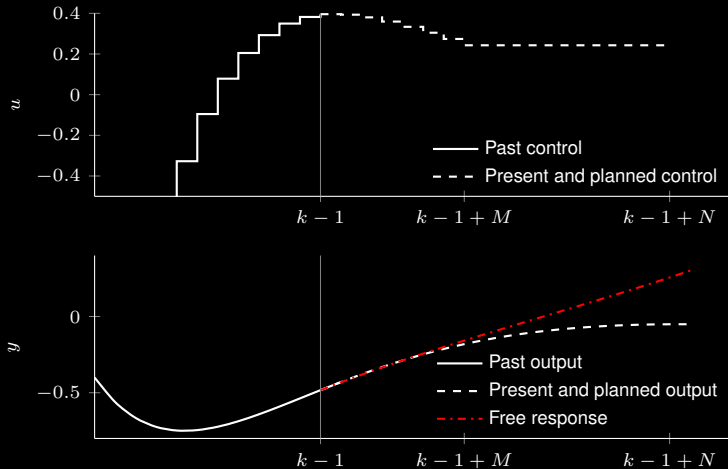


# An illustration of a receding horizon control



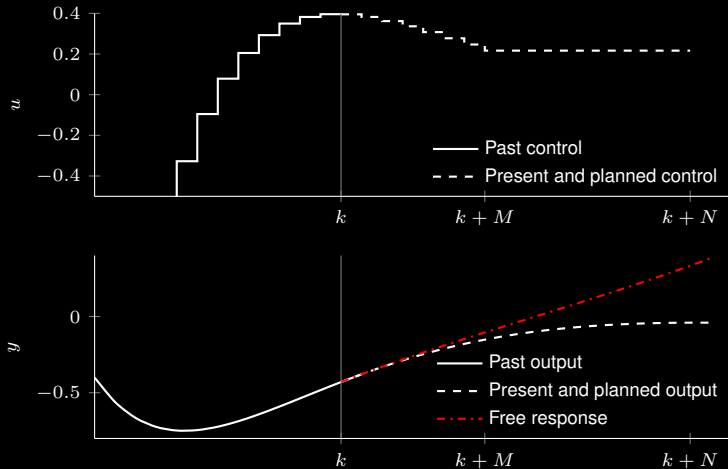
**Figure 4:** An illustration of a receding horizon control. The free response is the future response when the control signal stays at its current level.

# An illustration of a receding horizon control



**Figure 4:** An illustration of a receding horizon control. The free response is the future response when the control signal stays at its current level.

# An illustration of a receding horizon control



**Figure 4:** An illustration of a receding horizon control. The free response is the future response when the control signal stays at its current level.

## Example: Receding horizon control of an integrator system

- **System** at time  $k$ , with output dynamics:  $y(k+1) = y(k) + u(k)$ .
- **Past inputs:**  $\{\dots, u(k-2), u(k-1)\}$ .
- $u(k+1|k)$ : **planned (future) control input** at time  $k+1$ , given information at time  $k$ .
- $\Delta u(k+1|k) = u(k+1|k) - u(k|k)$ : **control increment**.
- $\hat{y}(k+1|k)$ : **predicted output** at time  $k+1$  given information at time  $k$ .
- **Prediction horizon:**  $N = 2$ .
- $r(k)$ : a **reference signal** to be followed by the output.

## Example: Receding horizon control of an integrator system

- **System** at time  $k$ , with output dynamics:  $y(k+1) = y(k) + u(k)$ .
- **Past inputs:**  $\{\dots, u(k-2), u(k-1)\}$ .
- $u(k+1|k)$ : **planned (future) control input** at time  $k+1$ , given information at time  $k$ .
- $\Delta u(k+1|k) = u(k+1|k) - u(k|k)$ : **control increment**.
- $\hat{y}(k+1|k)$ : **predicted output** at time  $k+1$  given information at time  $k$ .
- **Prediction horizon:**  $N = 2$ .
- $r(k)$ : a **reference signal** to be followed by the output.

The predicted outputs can be written as:

$$\hat{y}(k+1|k) = y(k) + u(k|k) = y(k) + u(k-1) + \Delta u(k|k) = y_f(k+1|k) + \Delta u(k|k)$$

## Example: Receding horizon control of an integrator system

- **System** at time  $k$ , with output dynamics:  $y(k+1) = y(k) + u(k)$ .
- **Past inputs:**  $\{\dots, u(k-2), u(k-1)\}$ .
- $u(k+1|k)$ : **planned (future) control input** at time  $k+1$ , given information at time  $k$ .
- $\Delta u(k+1|k) = u(k+1|k) - u(k|k)$ : **control increment**.
- $\hat{y}(k+1|k)$ : **predicted output** at time  $k+1$  given information at time  $k$ .
- **Prediction horizon:**  $N = 2$ .
- $r(k)$ : a **reference signal** to be followed by the output.

The predicted outputs can be written as:

$$\hat{y}(k+1|k) = y(k) + u(k|k) = y(k) + u(k-1) + \Delta u(k|k) = y_f(k+1|k) + \Delta u(k|k)$$

$$\hat{y}(k+2|k) = y(k) + u(k|k) + u(k+1|k) = y(k) + 2u(k|k) + \Delta u(k+1|k)$$

## Example: Receding horizon control of an integrator system

- **System** at time  $k$ , with output dynamics:  $y(k+1) = y(k) + u(k)$ .
- **Past inputs:**  $\{\dots, u(k-2), u(k-1)\}$ .
- $u(k+1|k)$ : **planned (future) control input** at time  $k+1$ , given information at time  $k$ .
- $\Delta u(k+1|k) = u(k+1|k) - u(k|k)$ : **control increment**.
- $\hat{y}(k+1|k)$ : **predicted output** at time  $k+1$  given information at time  $k$ .
- **Prediction horizon:**  $N = 2$ .
- $r(k)$ : a **reference signal** to be followed by the output.

The predicted outputs can be written as:

$$\begin{aligned}\hat{y}(k+1|k) &= y(k) + u(k|k) = y(k) + u(k-1) + \Delta u(k|k) = y_f(k+1|k) + \Delta u(k|k) \\ \hat{y}(k+2|k) &= y(k) + u(k|k) + u(k+1|k) = y(k) + 2u(k|k) + \Delta u(k+1|k) \\ &= y(k) + 2u(k-1) + 2\Delta u(k|k) + \Delta u(k+1|k)\end{aligned}$$

## Example: Receding horizon control of an integrator system

- **System** at time  $k$ , with output dynamics:  $y(k+1) = y(k) + u(k)$ .
- **Past inputs:**  $\{\dots, u(k-2), u(k-1)\}$ .
- $u(k+1|k)$ : **planned (future) control input** at time  $k+1$ , given information at time  $k$ .
- $\Delta u(k+1|k) = u(k+1|k) - u(k|k)$ : **control increment**.
- $\hat{y}(k+1|k)$ : **predicted output** at time  $k+1$  given information at time  $k$ .
- **Prediction horizon:**  $N = 2$ .
- $r(k)$ : a **reference signal** to be followed by the output.

The predicted outputs can be written as:

$$\begin{aligned}\hat{y}(k+1|k) &= y(k) + u(k|k) = y(k) + u(k-1) + \Delta u(k|k) = y_f(k+1|k) + \Delta u(k|k) \\ \hat{y}(k+2|k) &= y(k) + u(k|k) + u(k+1|k) = y(k) + 2u(k|k) + \Delta u(k+1|k) \\ &= y(k) + 2u(k-1) + 2\Delta u(k|k) + \Delta u(k+1|k) \\ &= y_f(k+2|k) + 2\Delta u(k|k) + \Delta u(k+1|k)\end{aligned}$$



## Example: Receding horizon control of an integrator system

- **System** at time  $k$ , with output dynamics:  $y(k+1) = y(k) + u(k)$ .
- **Past inputs:**  $\{\dots, u(k-2), u(k-1)\}$ .
- $u(k+1|k)$ : **planned (future) control input** at time  $k+1$ , given information at time  $k$ .
- $\Delta u(k+1|k) = u(k+1|k) - u(k|k)$ : **control increment**.
- $\hat{y}(k+1|k)$ : **predicted output** at time  $k+1$  given information at time  $k$ .
- **Prediction horizon:**  $N = 2$ .
- $r(k)$ : a **reference signal** to be followed by the output.

The predicted outputs can be written as:

$$\begin{aligned}\hat{y}(k+1|k) &= y(k) + u(k|k) = y(k) + u(k-1) + \Delta u(k|k) = y_f(k+1|k) + \Delta u(k|k) \\ \hat{y}(k+2|k) &= y(k) + u(k|k) + u(k+1|k) = y(k) + 2u(k|k) + \Delta u(k+1|k) \\ &= y(k) + 2u(k-1) + 2\Delta u(k|k) + \Delta u(k+1|k) \\ &= y_f(k+2|k) + 2\Delta u(k|k) + \Delta u(k+1|k)\end{aligned}$$

where  $y_f(\cdot|k)$  is the **free response**, i.e. the predicted output if the control input is frozen at time  $k$  to its last value  $u(k-1)$ .

## Case 1: control horizon of $M = 1$

Only one future control input is to be chosen, and we assume that the control stays constant after that, i.e.  $\Delta u(k+1|k) = 0$ . A natural criterion for having future outputs close to the reference signal

$$\begin{aligned} V_2 &= (\hat{y}(k+1|k) - r(k+1))^2 + (\hat{y}(k+2|k) - r(k+2))^2 \\ &= (y_f(k+1|k) + \Delta u(k|k) - r(k+1))^2 + (y_f(k+2|k) + 2\Delta u(k|k) - r(k+2))^2. \end{aligned}$$

## Case 1: control horizon of $M = 1$

Only one future control input is to be chosen, and we assume that the control stays constant after that, i.e.  $\Delta u(k+1|k) = 0$ . A natural criterion for having future outputs close to the reference signal

$$\begin{aligned} V_2 &= (\hat{y}(k+1|k) - r(k+1))^2 + (\hat{y}(k+2|k) - r(k+2))^2 \\ &= (y_f(k+1|k) + \Delta u(k|k) - r(k+1))^2 + (y_f(k+2|k) + 2\Delta u(k|k) - r(k+2))^2. \end{aligned}$$

We can solve for the optimal value by differentiating  $V_2$ , and set the derivative equal to zero:

$$\frac{\partial V_2}{\partial \Delta u(k|k)} = 2(y_f(k+1|k) + \Delta u(k|k) - r(k+1)) + 2(y_f(k+2|k) + 2\Delta u(k|k) - r(k+2)) \cdot 2 = 0.$$

## Case 1: control horizon of $M = 1$

Only one future control input is to be chosen, and we assume that the control stays constant after that, i.e.  $\Delta u(k+1|k) = 0$ . A natural criterion for having future outputs close to the reference signal

$$\begin{aligned} V_2 &= (\hat{y}(k+1|k) - r(k+1))^2 + (\hat{y}(k+2|k) - r(k+2))^2 \\ &= (y_f(k+1|k) + \Delta u(k|k) - r(k+1))^2 + (y_f(k+2|k) + 2\Delta u(k|k) - r(k+2))^2. \end{aligned}$$

We can solve for the optimal value by differentiating  $V_2$ , and set the derivative equal to zero:

$$\frac{\partial V_2}{\partial \Delta u(k|k)} = 2(y_f(k+1|k) + \Delta u(k|k) - r(k+1)) + 2(y_f(k+2|k) + 2\Delta u(k|k) - r(k+2)) \cdot 2 = 0.$$

This gives the optimal (incremental) control (remember that  $u(k) = u(k-1) + \Delta u(k|k)$ )

$$\Delta u(k|k) = \frac{1}{5} ((r(k+1) - y_f(k+1|k)) + 2(r(k+2) - y_f(k+2|k))). \quad (1)$$

Alternatively, we could describe this procedure as trying to solve the system of linear equations

$$\begin{cases} \hat{y}(k+1|k) = y_f(k+1|k) + \Delta u(k|k) = r(k+1) \\ \hat{y}(k+2|k) = y_f(k+2|k) + 2\Delta u(k|k) = r(k+2) \end{cases}$$

Alternatively, we could describe this procedure as trying to solve the system of linear equations

$$\begin{cases} \hat{y}(k+1|k) = y_f(k+1|k) + \Delta u(k|k) = r(k+1) \\ \hat{y}(k+2|k) = y_f(k+2|k) + 2\Delta u(k|k) = r(k+2) \end{cases}$$

or, using vector notation,

$$\begin{bmatrix} y_f(k+1|k) \\ y_f(k+2|k) \end{bmatrix} + \begin{bmatrix} 1 \\ 2 \end{bmatrix} \Delta u(k|k) = \begin{bmatrix} r(k+1) \\ r(k+2) \end{bmatrix} \Leftrightarrow$$

$$\mathbf{y}_f + \Theta \Delta u(k|k) = \mathbf{r}.$$

Alternatively, we could describe this procedure as trying to solve the system of linear equations

$$\begin{cases} \hat{y}(k+1|k) = y_f(k+1|k) + \Delta u(k|k) = r(k+1) \\ \hat{y}(k+2|k) = y_f(k+2|k) + 2\Delta u(k|k) = r(k+2) \end{cases}$$

or, using vector notation,

$$\begin{bmatrix} y_f(k+1|k) \\ y_f(k+2|k) \end{bmatrix} + \begin{bmatrix} 1 \\ 2 \end{bmatrix} \Delta u(k|k) = \begin{bmatrix} r(k+1) \\ r(k+2) \end{bmatrix} \Leftrightarrow$$

$$\mathbf{y}_f + \Theta \Delta u(k|k) = \mathbf{r}.$$

Since there is only one variable to fulfil two conditions, a natural solution is to find the value of  $\Delta u(k|k)$  that solves this system of linear equations in a least-squares sense, i.e. by minimizing  $\|\Theta \Delta u(k|k) - (\mathbf{r} - \mathbf{y}_f)\|^2$ . Expressing this in Matlab notation gives

$$\Delta u(k|k) = \Theta \backslash (\mathbf{r} - \mathbf{y}_f) = (\Theta^\top \Theta)^{-1} \Theta^\top (\mathbf{r} - \mathbf{y}_f), \quad (2)$$

which is identical to the solution (1).

## Case 2: control horizon of $M = 2$

There are two free variables. Hence, with the system of linear equations interpretation, the conditions to be fulfilled now become

$$\begin{bmatrix} y_f(k+1|k) \\ y_f(k+2|k) \end{bmatrix} + \begin{bmatrix} 1 & 0 \\ 2 & 1 \end{bmatrix} \begin{bmatrix} \Delta u(k|k) \\ \Delta u(k+1|k) \end{bmatrix} = \begin{bmatrix} r(k+1) \\ r(k+2) \end{bmatrix}$$



## Case 2: control horizon of $M = 2$

There are two free variables. Hence, with the system of linear equations interpretation, the conditions to be fulfilled now become

$$\begin{bmatrix} y_f(k+1|k) \\ y_f(k+2|k) \end{bmatrix} + \begin{bmatrix} 1 & 0 \\ 2 & 1 \end{bmatrix} \begin{bmatrix} \Delta u(k|k) \\ \Delta u(k+1|k) \end{bmatrix} = \begin{bmatrix} r(k+1) \\ r(k+2) \end{bmatrix}$$

which can now be solved uniquely for the optimal control sequence:

$$\begin{bmatrix} \Delta u(k|k) \\ \Delta u(k+1|k) \end{bmatrix} = \begin{bmatrix} 1 & 0 \\ 2 & 1 \end{bmatrix}^{-1} (\mathbf{r} - \mathbf{y}_f). \quad (3)$$

## Case 2: control horizon of $M = 2$

There are two free variables. Hence, with the system of linear equations interpretation, the conditions to be fulfilled now become

$$\begin{bmatrix} y_f(k+1|k) \\ y_f(k+2|k) \end{bmatrix} + \begin{bmatrix} 1 & 0 \\ 2 & 1 \end{bmatrix} \begin{bmatrix} \Delta u(k|k) \\ \Delta u(k+1|k) \end{bmatrix} = \begin{bmatrix} r(k+1) \\ r(k+2) \end{bmatrix}$$

which can now be solved uniquely for the optimal control sequence:

$$\begin{bmatrix} \Delta u(k|k) \\ \Delta u(k+1|k) \end{bmatrix} = \begin{bmatrix} 1 & 0 \\ 2 & 1 \end{bmatrix}^{-1} (\mathbf{r} - \mathbf{y}_f). \quad (3)$$

Sticking to the receding horizon principle, only the first element in the optimal control sequence is used, namely  $\Delta u(k|k)$ , and the other element is discarded.

# Summary

The MPC recipe for the example:

- a) At time  $k$ , predict the output  $N$  samples ahead:

$$\hat{y}(k+1|k), \dots, \hat{y}(k+N|k).$$

## Summary

The MPC recipe for the example:

- a) At time  $k$ , predict the output  $N$  samples ahead:

$$\hat{y}(k+1|k), \dots, \hat{y}(k+N|k).$$

- b) The predictions depend on future control inputs

$$u(k|k), u(k+1|k), \dots, u(k+M-1|k).$$

(Normally,  $M \leq N$ , and we assume that  $u$  is either 0 or unchanged after this.)

## Summary

The MPC recipe for the example:

- a) At time  $k$ , predict the output  $N$  samples ahead:

$$\hat{y}(k+1|k), \dots, \hat{y}(k+N|k).$$

- b) The predictions depend on future control inputs

$$u(k|k), u(k+1|k), \dots, u(k+M-1|k).$$

(Normally,  $M \leq N$ , and we assume that  $u$  is either 0 or unchanged after this.)

- c) Minimize a criterion (now adopting the index notation as in Matlab)

$$V(k) = V(\hat{y}(k+1:k+N|k), u(k:k+M-1|k))$$

with respect to the control sequence  $u(k:k+M-1|k)$ .

# Summary

The MPC recipe for the example:

- a) At time  $k$ , predict the output  $N$  samples ahead:

$$\hat{y}(k+1|k), \dots, \hat{y}(k+N|k).$$

- b) The predictions depend on future control inputs

$$u(k|k), u(k+1|k), \dots, u(k+M-1|k).$$

(Normally,  $M \leq N$ , and we assume that  $u$  is either 0 or unchanged after this.)

- c) Minimize a criterion (now adopting the index notation as in Matlab)

$$V(k) = V(\hat{y}(k+1:k+N|k), u(k:k+M-1|k))$$

with respect to the control sequence  $u(k:k+M-1|k)$ .

- d) Apply the first control signal in the sequence to the process:

$$u(k) = u(k|k).$$

# Summary

The MPC recipe for the example:

- a) At time  $k$ , predict the output  $N$  samples ahead:

$$\hat{y}(k+1|k), \dots, \hat{y}(k+N|k).$$

- b) The predictions depend on future control inputs

$$u(k|k), u(k+1|k), \dots, u(k+M-1|k).$$

(Normally,  $M \leq N$ , and we assume that  $u$  is either 0 or unchanged after this.)

- c) Minimize a criterion (now adopting the index notation as in Matlab)

$$V(k) = V(\hat{y}(k+1:k+N|k), u(k:k+M-1|k))$$

with respect to the control sequence  $u(k:k+M-1|k)$ .

- d) Apply the first control signal in the sequence to the process:

$$u(k) = u(k|k).$$

- e) Increment time  $k := k+1$  and go to 1.

# MPC ingredients

- An **internal model** describing process and disturbances.
- An **estimator/predictor** to determine the evolution of the state.
- An **objective/criterion** to express the desired system behaviour.
- An **online optimisation algorithm** to determine future control actions.
- The **receding horizon** principle.
- Our focus: linear models, quadratic criteria with linear constraints.



# Outline of the course

- What is MPC? Introduction, motivation and review.
- MPC basics and relations to dynamic programming.
- How to cope with incomplete state information.
- Solving predictive control problems.
- User aspects, case study, guest lecture.
- MPC theory.
- Review and outlook.

# Learning objectives

After completion of the course, you should be able to:

- Understand and explain the basic principles of model predictive control, its pros and cons, and the challenges met in implementation and applications.
- Correctly state, in mathematical form, MPC formulations of control problems in various applications.
- Describe and construct MPC controllers based on a linear model, quadratic costs and linear constraints.
- Describe basic properties of MPC controllers and analyse algorithmic details on simple examples.
- Understand and explain basic properties of the optimisation problem as an ingredient of MPC, in particular concepts like linear, quadratic and convex optimisation, optimality conditions, and feasibility.
- Use software tools for analysis and synthesis of MPC controllers.

## Practical information

- Canvas: syllabus, news, schedule, assignments and more...
- Literature.
- Lectures: slides and Lecture Notes. Lectures will be recorded.
- Problem solving sessions: analytical problems + Matlab coding.
- Home assignments.
- Micro assignments.
- Examination.
- Course representatives.

# Literature

- *Model Predictive Control, Lecture Notes.*
- J.B. Rawlings, D.Q. Mayne, M.M. Diehl: *Model Predictive Control. Theory, Computation, and Design*, 2nd ed. Amazon or online.
- Supplementary literature suggested at the course homepage.
- Also @Canvas: Assignments, Matlab files, etc.

# Home and micro assignments

There are **7 mandatory home assignments** and 1 optional. The home assignments constitute the main part of the examination in the course and should be pursued **individually**.

Note:

- Read the instructions carefully.
- Start working early to meet deadlines.
- Use Supervision sessions to get help.

# Home and micro assignments

There are **7 mandatory home assignments** and 1 optional. The home assignments constitute the main part of the examination in the course and should be pursued **individually**.

Note:

- Read the instructions carefully.
- Start working early to meet deadlines.
- Use Supervision sessions to get help.

There are also **13 compulsory micro-assignments** to be completed before each lecture.

- They are designed in the form of quizzes, to be completed online, on Canvas.
- Each micro-assignment gives maximum of 2 points.
- At least 18 points are needed in order to pass the course.

## Grading scheme for home assignments

- Each assignment gives maximum 15 points, except assignment 1 that gives max 10 points.
- The seven compulsory assignments thus give in total max 100 points.
- The optional assignment 8 can give additional 15 points.
- The total score decides the grade with limits 40, 60, 80 points.
- To ensure enough coverage of the course, a minimum of 5 points is required for each of at least 6 assignments.

Each assignment has a deadline. Possible late submissions are handled in the following way:

- A cumulative "delay budget" of max 5 days is available for each student.
- Total delay within this limit will not affect the score, but once the limit is reached, assignments submitted late will render 0 points, as will any assignment submitted more than 3 days late.

# Course representatives

The following student representatives will participate in the course evaluation:

- Alfred Hazard
- Subramanya Mallappa
- Nathaly Sanchez Chan
- Pramod Sivaramakrishnan
- Ahmad Wahba



# References

- [1] J.B. Rawlings, D.Q. Mayne, and M.M. Diehl. *Model Predictive Control: Theory, Computation, and Design, 2nd edition*. Nob Hill Publishing 2017.  
Available online at <https://sites.engineering.ucsb.edu/~jbraw/mpc>
- [2] G. Goodwin, M.M. Seron, and J.A. De Don. *Constrained Control and Estimation*. Springer 2004.  
Available online via Chalmers Library.
- [3] F Borrelli, A. Bemporad, and M. Morari. *Predictive Control for Linear and Hybrid Systems*.  
Available online at <http://www.mpc.berkeley.edu/mpc-course-material>
- [4] J. Maciejowski. *Predictive Control with Constraints*. Prentice Hall 2002.
- [5] S. Boyd and L. Vandenberghe. *Convex optimisation*. Cambridge University Press 2004.
- [6] Diehl, M. *Real-Time Optimization for Large Scale Nonlinear Processes*. PhD thesis, University of Heidelberg, 2001.



**CHALMERS**  
UNIVERSITY OF TECHNOLOGY