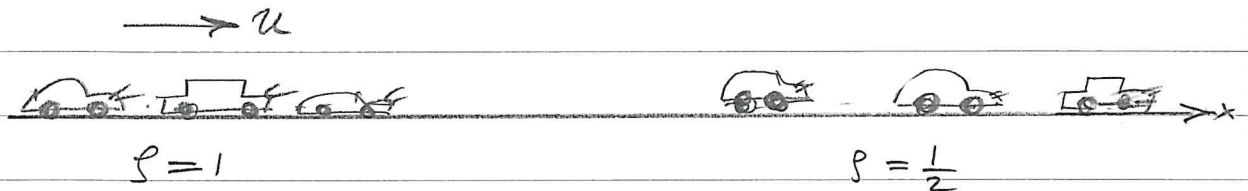


Example; The traffic flow in a highway:



Let $\rho = \rho(x, t)$ be the density of cars ($0 \leq \rho \leq 1$) and $u = u(x, t)$ the velocity (speed vector) of the cars.

For a highway path (a, b) the difference between the traffic inflow $u(a)\rho(a)$ at the point $x=a$ and outflow $u(b)\rho(b)$ at $x=b$ gives the density variation on the interval (a, b) :

$$\frac{d}{dt} \left(\int_a^b \rho(x, t) dx \right) = \int_a^b \dot{\rho}(x, t) dx = \rho(a)u(a) - \rho(b)u(b) = - \int_a^b (u\rho)' dx.$$

$$\Leftrightarrow \int_a^b \{ \dot{\rho} + (u\rho)' \} dx = 0.$$

Since a & b can be chosen arbitrary. Thus

$$(*) \quad \underline{\dot{\rho} + (u\rho)' = 0}.$$

Let now $u = 1 - \rho$ (motivate) then $\dot{\rho} + ((1-\rho)\rho)' = 0$,

i.e.

$$\boxed{\dot{\rho} + (1-2\rho)\rho' = 0}$$



A non-linear convection-equation

As an alternative let now $u = C - \varepsilon (f'/f)$ in (x), $C > 0$, $\varepsilon > 0$, (motivate). Then we get

$$f'' + \left((C - \varepsilon \frac{f'}{f}) f \right)' = 0 \Rightarrow \underline{f'' + C f' - \varepsilon f'' = 0.}$$

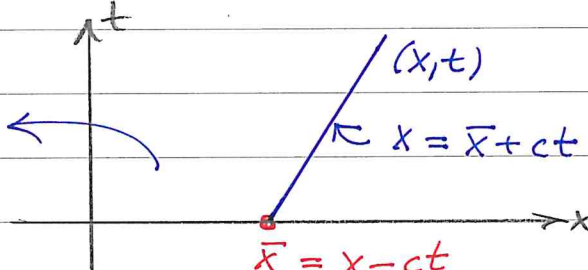
i.e., A time dependent convection-diffusion equation
(convection dominated if $C > \varepsilon$)

For $\varepsilon = 0$ the solution is given by the exact transport:

$$f(x, t) = f_0(x - ct), \text{ because then } f = \text{constant on the}$$

$(C, 1)$ - direction:

$$\Leftrightarrow (C, 1) \cdot \left(\frac{\partial f}{\partial x}, \frac{\partial f}{\partial t} \right) = 0;$$

$$\left(\begin{array}{l} f(x, t) = f(\bar{x} + ct, t) \\ \frac{\partial f}{\partial x} \frac{\partial x}{\partial t} + \frac{\partial f}{\partial t} = 0 \Rightarrow \\ C f' + f'' = 0 \dots \end{array} \right)$$


Change of notation $f \Rightarrow u \xrightarrow{C \gg \beta} \underline{\dot{u} + \beta u' - \varepsilon u'' = 0.}$

Compare to the Navier-Stokes equation for incompressible flow:

$$\begin{cases} \dot{u} + (\beta \cdot \nabla) u - \varepsilon \Delta u + \Delta p \equiv 0 \\ \text{div } u = 0 \end{cases}$$

where $\beta = u$, $\underline{u} = \overset{\text{mass}}{(u_1, u_2, u_3)}$ is the velocity vector,
 $\uparrow$ $\uparrow$
 momentum energy

p is the pressure and $\varepsilon = \frac{1}{\text{Re}}$, with Re being the Reynolds' number.

These equations are not easily solvable for $\varepsilon > 0$ small, because of boundary layer and turbulence. A typical range of Re is between 10^5 and 10^7 .

An example of stationary convection-diffusion (Boundary layer problem)

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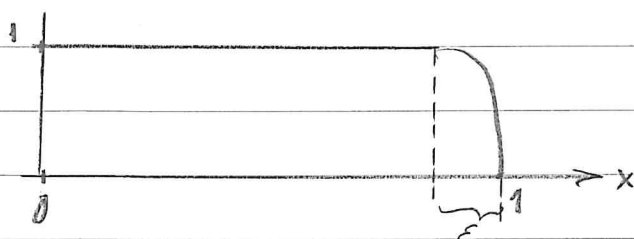
HA.

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Example Consider the (BVP):
$$\begin{cases} u' - \varepsilon u'' = 0, & 0 < x < 1 \\ u(0) = 1, & u(1) = 0. \end{cases}$$

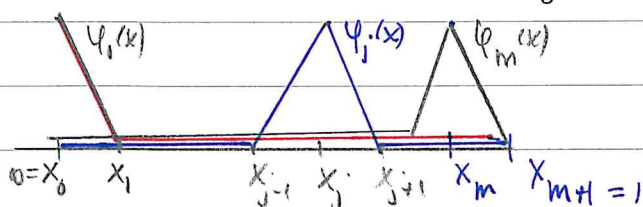
The exact solution is given by

$$u(x) = c \left(e^{\frac{x}{\varepsilon}} - e^{\frac{1-x}{\varepsilon}} \right), \quad \text{with } c = \frac{1}{\left(e^{\frac{1}{\varepsilon}} - 1 \right)}.$$



Note an outflow
boundary layer
of width $\sim \varepsilon$

FEM. Set $U(x) = \varphi_0(x) + U_1 \varphi_1(x) + \dots + U_m \varphi_m(x)$



Inserting in corresponding
discrete variational formulation:

$$\left(\begin{matrix} C \\ \text{is} \\ \text{convection} \\ \text{matrix} \end{matrix} \right) \quad \int_0^1 U' \varphi_j + \varepsilon \int_0^1 U' \varphi_j' = 0, \quad j=1, \dots, m$$

yields (row j): $\int_0^1 \varphi_j' \varphi_j = 0, \quad \int_0^1 \varphi_{j-1}' \varphi_j = -\frac{1}{2}, \quad \int_0^1 \varphi_{j+1}' \varphi_j = \frac{1}{2}$

$$(**) \quad \frac{1}{2} (U_{j+1} - U_{j-1}) + \frac{\varepsilon}{h} (2U_j - U_{j-1} - U_{j+1}) = 0, \quad j=1, \dots, m$$

where $U_0 = 1$ & $U_{m+1} = 0$

Notice that we can also use central-differencing
and write:

$$\underbrace{\frac{U_{j+1} - U_{j-1}}{2h}}_{\text{Corresp. to } U'(x_j)} - \varepsilon \underbrace{\frac{U_{j+1} - 2U_j + U_{j-1}}{h^2}}_{\text{Corresp. to } U''(x_j)} = 0 \quad \left(\begin{matrix} \text{OBS!} \\ \text{(**)} \\ h \end{matrix} \right)$$

For ε very small this gives that $U_{j+1} \approx U_{j-1}$, given, for even m values alternating 0 and 1 as the solution values at the nodes:

Oscillatory behavior of convection dominated problem. [The streamline diffusion method] -4-

JAA.

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i.e. Oscillation in u are transported "upstream" making u a globally "bad" approximation of u .

A better way is to approximate $u'(x_j)$ by an "upwind" derivative:

$$u'(x_j) \approx \frac{u_j - u_{j-1}}{h},$$

which, formally, gives a better stability, however with low accuracy. The example itself demonstrates that a high accuracy without stability is indeed useless.

A more systematic method of making FE-solution of the fluid problems stable; is through using:

The Streamline-diffusion method (SDM):

The idea is to choose the test functions of the form

$$(v + \frac{1}{2} \beta h v'), \quad \text{instead of just } v.$$

Then, e.g., for our model problem (example above) we obtain ($\beta=1$) the variational formulation: with source $f(x)$

$$(VF) \quad \int_0^1 [u'(v + \frac{1}{2} h v') - \varepsilon u''(v + \frac{1}{2} h v')] dx = \int_0^1 f(v + \frac{1}{2} h v') dx.$$

Here in the discrete version of the variational formulation, one should interpret the term $\int_0^1 u'' v' dx$ as

$$\sum_j \int_{T_j} u'' v' \quad (=0 \text{ in case of approx. with P.L.})$$

cont.

The Streamline-diffusion method (SDM)

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Note that with $v = \varphi_j$ in discrete version of (VF):

$$\int_0^1 U' \frac{1}{2} h \varphi_j' = U_j - \frac{1}{2} U_{j+1} - \frac{1}{2} U_{j-1} \quad \text{combined with (stiffness matrix row j)}$$

$$\int_0^1 U' \varphi_j = \frac{U_{j+1} - U_{j-1}}{2} \quad (\text{conv. matrix row j})$$

gives $(U_j - U_{j-1})$ approx. the 1st integral in (VF), corresponding to the upwind scheme.

The SDM can also be interpreted as a sort of least-square.

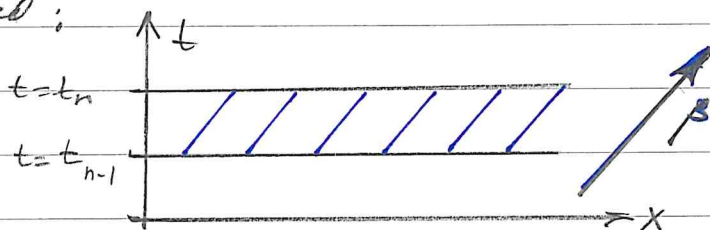
Let $A = \frac{d}{dx}$, $A^t = -\frac{d}{dx}$, then u minimizes

$$\|w' - f\| \quad \text{if } u' = Au = f \Leftrightarrow A^t Au = A^t f$$

$$\Leftrightarrow \{ \text{mult. } v \in \{ \} \} \Leftrightarrow -u'' = (-f' = g) \quad (\text{continuous})$$

$$\Leftrightarrow \left\{ \begin{array}{l} \int \beta I \text{ in both sides} \\ \text{with Dirichlet data} \end{array} \right\} \Leftrightarrow \int U' v' = \int f v' \quad (\text{weak form}).$$

For the time dependent convection problem, the oriented space-time elements are used:



Set $U(x, t)$ such that U is piecewise-linear in x and piecewise constant in the $(\beta, 1)$ -direction. Combine with SDM and add up some artificial viscosity $\hat{\epsilon}$ depending on the residual term to get for each time interval:

$$\int_{I_n} \int_{\Omega} \{ (u + \beta u) (v + \frac{\beta}{2} h v) + \hat{\epsilon} U' v' \} = \int_{I_n} \int_{\Omega} \{ f (v + \frac{\beta}{2} h v) \} \dots$$